



# Kinetic and equilibrium studies for the adsorption process of cadmium(II) and copper(II) onto *Pseudomonas aeruginosa* using square wave anodic stripping voltammetry method

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## ABSTRACT

A novel method for the simultaneous determination of cadmium(II) and copper(II) during the adsorption process onto *Pseudomonas aeruginosa* was developed. The concentration of the free metal ions was successfully detected by square wave anodic stripping voltammetry (SWASV) on the mercaptoethane sulfonate (MES) modified gold electrode, while the *P. aeruginosa* was efficiently avoided approaching to the electrode surface by the MES monolayer. And the anodic stripping peaks of Cd<sup>2+</sup> and Cu<sup>2+</sup> appear at -0.13 and 0.34 V respectively, at the concentration range of 5–50 μM, the peak currents of SWASV present linear relationships with the concentrations of cadmium and copper respectively. As the determination of Cd<sup>2+</sup> and Cu<sup>2+</sup> was in real time and without pretreatment, the kinetic characteristics of the adsorption process were studied and all the corresponding regression parameters were obtained by fitting the electrochemical experimental data to the pseudo-second-order kinetic model. Moreover, Langmuir and Freundlich models well described the biosorption isotherms. And there were some differences in the amount of metal ion adsorbed at equilibrium ( $q_e$ ) and other kinetics parameters when the two ions coexisted were compared with the unaccompanied condition, which were also discussed in this paper. The proposed electrode system provides excellent platform for the simultaneous determination of trace metals in complex biosorption process.

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## 1. Introduction

The water environment has been contaminated by persistent pollutants of agriculture and industrial origin during recent decades. Heavy metal contamination has serious impact on the environment, due to discharges from industrial wastes, agricultural and urban sewage. Heavy metals can be accumulated by organisms through a variety of pathways, including respiration, adsorption and ingestion, which are highly toxic to many organs of both humans and animals [1,2]. The conventional methods used to treat wastewater containing heavy metals consist of chemical precipitation, solvent extraction, ion exchange, membrane processes, dialysis, carbon adsorption and so on [3,4]. However, most of the methods mentioned above are fussy in operation, frequently expensive, or inefficient at trace concentration. Thus, it is very desirable to develop a rapid, simple, reliable method for treating such toxic metal ions. Biosorption using microbes is a cost-effective approach to remove heavy metals in the industrial effluents [5]. The main advantages of this technique are the

reusability of biomaterial, low operating cost, improved selectivity for specific metals of interest, removal of heavy metals from effluent irrespective of toxicity, and no production of secondary compounds which might be toxic [6,7]. *Pseudomonas aeruginosa* (*P. aeruginosa*) is widely used for its advantages in high efficiency of biosorption performance and low operating cost [8,9]; while the inactive biosorption of metal by microbe is focused as well [10].

Anodic stripping voltammetry (ASV) is regarded as a highly sensitive, accurate and convenient technique for trace metal analysis, which is fit for simultaneous analysis of metal ions [11–13]. In order to avoid organic macromolecular polluting the electrode surface [14,15], which can lead to the electrode activity loss and reduced sensitivity, a porous film should be modified on the electrode surface. And the self-assembly of mercaptoethane sulfonate (MES) on the gold electrode surface was successfully used for the detection of trace metal ion in the presence of *P. aeruginosa* cells [16]. Thus, the gold electrode modified by MES can be used to directly determine the copper and cadmium ions simultaneously. Moreover, compared to the conventional techniques determining the metal ions during the biosorption process such as gravimetry, colorimetry and atomic absorption spectrophotometry [17,18], ASV not only shuns the bothers of pretreatment and time-consuming, but also can offer

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the real-time information for the study of the biosorption kinetics process.

In this paper, square wave anodic stripping voltammetry (SWASV) at MES monolayer modified electrode was first used for the simultaneous monitoring that copper(II) and cadmium(II) adsorbed onto the nonliving biomass of *P. aeruginosa*. The porous disorganized monolayer formed by MES prevents the contaminants *P. aeruginosa* fouling the gold electrode surface, while the free metal ions can penetrate through the monolayer to be determined by the voltammetric detector. The concentrations of the free  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  would be detected by SWASV each 2–5 min until the biosorption equilibrium approaches. Based on the electrochemical results, the adsorption kinetics and isothermal models were investigated.

## 2. Material and methods

### 2.1. Reagents

Mercaptoethane sulfonate (MES, purity  $\geq 99\%$ ) was purchased from Sigma–Aldrich (St. Louis, MO, USA). Beef extract and peptone were obtained from Shanghai Reagent Factory (Shanghai, China). Experimental solutions of cadmium and copper ions were respectively prepared by diluting  $1 \times 10^{-3}$  M of cadmium and copper stock solutions, which were obtained by dissolving corresponding chlorides into doubly distilled water. All of the other reagents were of analytical reagent grade and were used without further purification. Doubly distilled water was used throughout.

### 2.2. Apparatus

The electrochemical measurements were carried out in a conventional three-electrode detected cell on a CHI 660 A electrochemical workstation (Shanghai Chenhua Apparatus Co., Shanghai, China) with CHI software, connecting to a personal computer. An MES-modified gold electrode (2 mm in diameter) was used as the working electrode, a platinum wire auxiliary electrode, and a saturated calomel electrode (SCE) was used as the reference electrode. All potentials were vs. the reference electrode. A magnetic stirrer (Model 79-1, Shanghai Hexin Technique and Education Equipment Co., Shanghai, China) was employed to stir the testing solution during the biosorption process of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  onto *P. aeruginosa*.

### 2.3. Bacterial solution and preparation of biosorbent

*P. aeruginosa* was purchased from Medical School of Central South University (Changsha, China). The composition of the broth medium for *P. aeruginosa* was as follows: beef extract, 5.0 g; peptone, 10.0 g; sodium chloride, 5.0 g; distilled water, 1000 ml. Then 0.1 M NaOH use used to adjust the value of pH to 7.2. The medium was sterilized by autoclaving at  $121^\circ\text{C}$  for 15 min. Inoculate four loops of *P. aeruginosa* from an agar slant medium into a 250 ml sterilized conical glass flasks containing 100 ml sterilized broth culture medium, incubated at  $37^\circ\text{C}$  with gentle oscillation for 24 h. After that, the cells were gathered by centrifugation at the rotating speed of 11,000 rpm for 20 min and the cells were washed twice with double distilled water. Then the cells were dried at  $80^\circ\text{C}$  for 24 h. In the phase of homogenizing, the dried cells were homogeneously dispersed in double-distilled and sterilized water by a homogenizer at 2500 rpm for 30 min, and then stored in the refrigerator at  $4^\circ\text{C}$  for further use.

### 2.4. Modification of electrode

#### 2.4.1. Pretreatment of the gold electrode

Before modification, the gold electrode was required to be polished carefully with  $0.3\ \mu\text{m}$  and  $0.05\ \mu\text{m}$   $\alpha$ -alumina powder

slurries on a 1200 grit Carbimet disk until a mirror shiny surface was obtained, and then immersed in an ultrasonic bath sequentially with ethanol double distilled water for 3 min to remove traces of alumina and possible contamination, and finally rinsed with double distilled water. Then the undefiled electrode was cycled from 0 to 1.5 V in 0.5 M  $\text{H}_2\text{SO}_4$  solution until stable cyclic voltammograms were obtained, and then rinsed adequately with double distilled water and dried with  $\text{N}_2$ .

#### 2.4.2. Self-assembling of MES

After the pretreatment, the electrode was modified by immersing in a solution mixed with 5 mM MES and 0.1 M perchloric acid at open circuit for 10 min [19]. Finally, the electrode was carefully rinsed with abundant amount of double distilled water, dried in  $\text{N}_2$  stream, and then immediately fixed into an electrochemical cell.

### 2.5. Testing procedure

The detector was constructed in the 10 ml testing cell with 0.1 M NaCl solution as the electrolyte and the prepared electrodes as the working electrodes. The biosorption experiments were performed by adding  $50\ \text{mg l}^{-1}$  (final concentration) of *P. aeruginosa* cells suspensions into the testing cell containing given amount of cadmium and copper ions. For the biosorption process, the free metal ions in the solution decreased which would be determined directly by SWASV, until the adsorption reached the equilibrium. The peak currents of cadmium and copper were recorded every 2–5 min. And the experimental electrochemical parameters were optimized and the optimal parameters were used as follows: increase potential, 10 mV; amplitude, 25 mV; frequency, 15 Hz; initial potential,  $-0.3\ \text{V}$ ; final potential,  $0.6\ \text{V}$ ; deposition potential,  $-0.3\ \text{V}$ ; deposition time, 10 s; quiet time, 2 s. All the electrochemical experiments were performed at room temperature ( $20^\circ\text{C}$ ).

## 3. Results and discussion

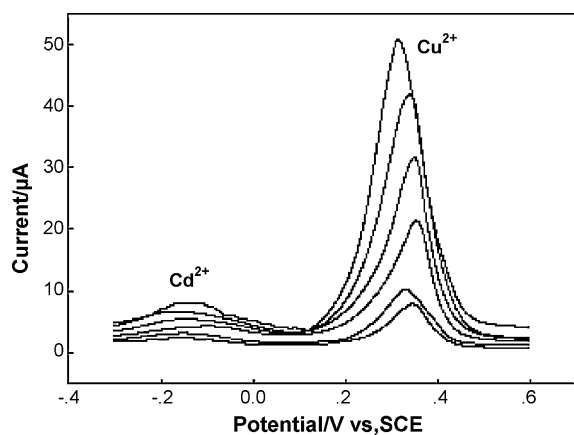
### 3.1. The SWASV characterization of $\text{Cd}^{2+}$ and $\text{Cu}^{2+}$ on the MES-modified electrode and the calibration plots

MES has only a two-carbon short chain and a highly charged group at one end (sulfonate group in solution). Such a structure can diminish the affinity between the alkyls border upon and augment the electrostatic repulsion between the endmost chain groups [20]. In this way, it is easy to form a disorganized and porous MES monolayer at the surface of the gold electrode [21], which can let small particulates such as metal ions permeate through while macromolecules like microbial cells and protein molecules would be held out due to their large size. Thus, the free ions  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  can be detected by the sensor and the electrode can not be polluted by *P. aeruginosa* cells. Besides, because MES monolayer film is electronegative, it can attract more metal ions onto the electrode surface in the anodic stripping voltammograms.

Fig. 1 shows the SWASV of cadmium and copper in the concentration range from 5 to  $50\ \mu\text{M}$  on the MES-modified gold electrode. The detection of metal ions is negligibly affected by the presence of *P. aeruginosa* in the solution [22]. The sustaining electrolyte is 0.1 M NaCl solution, and the stripping peaks of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  appear at  $-0.13$  and  $0.34\ \text{V}$  respectively. At the concentration range of  $5\text{--}50\ \mu\text{M}$ , the peak currents of SWASV present linear relationships with the concentrations (C) of cadmium and copper respectively. The linear regression equation is as follows:

$$i_p = aC + b \quad (1)$$

By fitting the experimentally obtained maximum of  $i_p$  shown as drops, the results are given as follows: for  $\text{Cd}^{2+}$ :  $a = 0.118\ \mu\text{A}\ \mu\text{M}^{-1}$ ,



**Fig. 1.** Square wave anodic stripping voltammograms (SWASV) of cadmium and copper in 0.1 M NaCl at mercaptoethane sulfonate-modified gold electrodes. The concentrations of cadmium and copper are 5, 10, 20, 30, 40 and 50  $\mu\text{M}$  from bottom to top.

$b = 0.0110 \mu\text{A}$ ,  $R^2 = 0.9979$ ; for  $\text{Cu}^{2+}$ :  $a = 1.0066 \mu\text{A} \mu\text{M}^{-1}$ ,  $b = -0.5418 \mu\text{A}$ ,  $R^2 = 0.9945$ .  $R^2$  is the correlative coefficient, and the values of  $R^2$  here imply that the response model can well describe the relationship between  $i_p$  and the concentrations of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$ .

### 3.2. Comparison of the proposed method with atomic absorption spectrometry

To verify the accuracy of the proposed method, the results obtained by this method were compared with that by atomic absorption spectrometry (AAS).  $5 \mu\text{M}$   $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  were added to 0.1 M NaCl solution contained  $25 \text{ mg l}^{-1}$  *P. aeruginosa* cells. The concentration of metal ions in the simulated sample was determined by the approach described above and AAS. The samples used in the latter case were pretreated to remove the *P. aeruginosa* cells. The results obtained were shown in Table 1. The concentrations of metal ions detected by this method were greater than those of AAS. This may be because some metal ions were absorbed by *P. aeruginosa* cells during the pretreatment. The result in Table 1 suggested the accuracy and reliability of this method. Moreover, this method avoided cumbersome operations, and could provide real-time information for monitoring of the biosorption process.

### 3.3. The dynamics model for the biosorption process of $\text{Cd}^{2+}$ and $\text{Cu}^{2+}$ onto *P. aeruginosa*

After *P. aeruginosa* cells were injected,  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  were adsorbed onto the nonliving microorganisms by virtue of the electrostatic interaction between metal ions and the anionic ligands in the lipopolysaccharide and other surface polymers [22]. To describe the characteristic for the efficiency of biosorption, a dynamics model should be discussed. The pseudo-second-order model was

**Table 1**

Comparison of this method (the sample without pretreatment) and atomic absorption spectrometry (the sample with pretreatment) for determination of  $\text{Cu}^{2+}$  and  $\text{Cd}^{2+}$  in the simulated sample contained  $25 \text{ mg l}^{-1}$  *P. aeruginosa* cells.

Ion	Detected by this method		Detected by AAS <sup>b</sup>	
	C ( $\mu\text{M}$ ) <sup>a</sup>	RSD <sup>c</sup> (n=5)	C ( $\mu\text{M}$ ) <sup>a</sup>	RSD <sup>c</sup> (n=5)
$\text{Cu}^{2+}$	4.43	4.94%	4.06	4.42%
$\text{Cd}^{2+}$	4.14	4.45%	3.63	4.58%

<sup>a</sup> Average of five determinations.

<sup>b</sup> AAS is atomic absorption spectrometry.

<sup>c</sup> RSD is relative standard derivation.

used well in adsorption studies, even in the study of biosorption process [16]. The equation of the pseudo-second-order kinetic model is expressed as follows:

$$\frac{dq_t}{dt} = k_2(q_e - q_t)^2 \quad (2)$$

where  $k_2$  is the rate constant of second-order adsorption ( $\text{mg} \mu\text{mol}^{-1} \text{min}^{-1}$ ),  $q_t$  ( $\mu\text{mol mg}^{-1}$ ) is the amount of metal ions adsorbed at time  $t$ , and  $q_e$  ( $\mu\text{mol mg}^{-1}$ ) is the amount of metal ion adsorbed at equilibrium.

The relationship of  $q_t$ ,  $t$ , metal ions concentration  $C$  ( $\mu\text{M}$ ) and the amount of biomass  $X$  ( $\text{mg l}^{-1}$ ) is shown in Eq. (3).

$$q_t = \frac{C_0 - C_t}{X} \quad (3)$$

$C_0$  and  $C_t$  ( $\mu\text{M}$ ) are the metal concentrations in the solution at initial and at time  $t$ , respectively. When  $t$  is equal to the equilibrium contact time, the concentration of the metal ions is equal to the concentration at equilibrium ( $C_e$ ), viz.  $C_t = C_e$ , and  $q_t = q_e$ .

Integrating Eqs. (1) and (3), a new equation is obtained, given by Eq. (4):

$$q_t = -\kappa \Delta i_p \quad (4)$$

where  $\Delta i_p$  ( $\mu\text{A}$ ) is defined as the discrepant value of  $i_p$  at time  $t$  vs. initial.  $\kappa$  ( $\mu\text{mol mg}^{-1} \mu\text{A}^{-1}$ ) is a coefficient. When  $t \rightarrow \infty$ , the adsorption dynamics go close to the equilibrium,  $i_p \rightarrow i_{p,\text{max}}$ ,  $q_t \rightarrow q_e$ . Eq. (4) can be replaced by Eq. (5):

$$q_e = -\kappa \Delta i_{p,\text{max}} \quad (5)$$

From Eqs. (2), (4) and (5), Eq. (6) is obtained:

$$\begin{aligned} -\frac{d\Delta i_p}{dt} &= \kappa k_2 (\Delta i_p - \Delta i_{p,\text{max}})^2 \\ &= k'_2 (\Delta i_p - \Delta i_{p,\text{max}})^2 \end{aligned} \quad (6)$$

Integrating Eq. (6), a new equation used to describe the relation between  $\Delta i_p$  and biosorption kinetics parameters is expressed as follows:

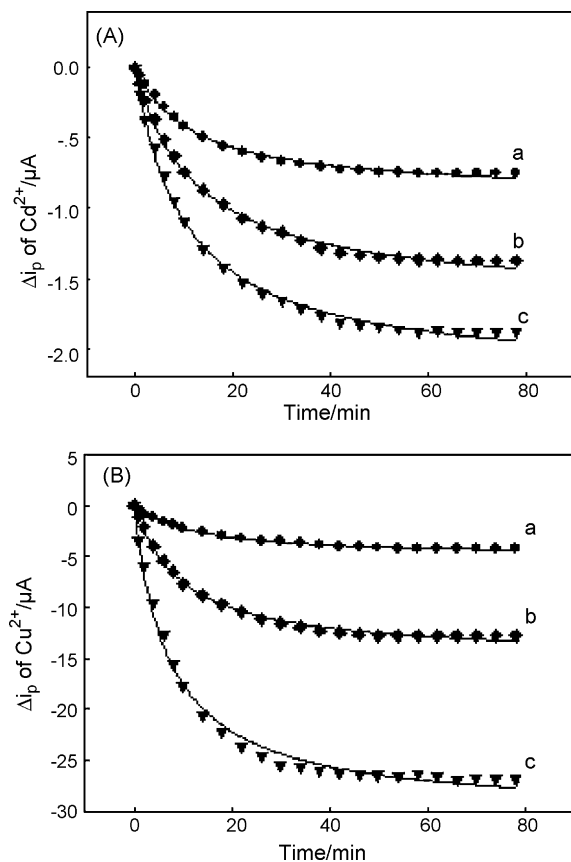
$$\Delta i_p = \frac{k'_2 \Delta i_{p,\text{max}}^2 t}{k'_2 \Delta i_{p,\text{max}} t - 1} \quad (7)$$

Eq. (7) is the right kinetics model for the biosorption process of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  onto *P. aeruginosa*.

### 3.4. The $\Delta i_p$ response of $\text{Cd}^{2+}$ and $\text{Cu}^{2+}$ on the MES-modified electrode during the biosorption process in the presence of either metal ions

After *P. aeruginosa* biomass solution was added into the electrochemical cell containing only one sort of detected ion such as  $\text{Cd}^{2+}$ , the typical  $\Delta i_p$  responses with time during the binding process of  $\text{Cd}^{2+}$  onto *P. aeruginosa* at different initial cadmium concentrations are shown in Fig. 2(A). From the adsorption curve in Fig. 2(A), it can be noted that  $\Delta i_p$  decreases rapidly during the initial 20 min, which corresponds to the fast adsorption period of *P. aeruginosa*, the value of  $\Delta i_p$  in this period can reach a 80 percent of the total. Then the declining rate of  $\Delta i_p$  slows and finally reaches a stable level forming a roof, and the adsorption process almost finishes. It can also be regarded that the biosorption course is rapid, and the nonliving *P. aeruginosa* cells must be a highly efficient sorbent.

In accordance with  $\text{Cd}^{2+}$ , the  $\Delta i_p$  response of  $\text{Cu}^{2+}$  adsorbed onto *P. aeruginosa* cells has the same changing trend, shown in Fig. 2(B).

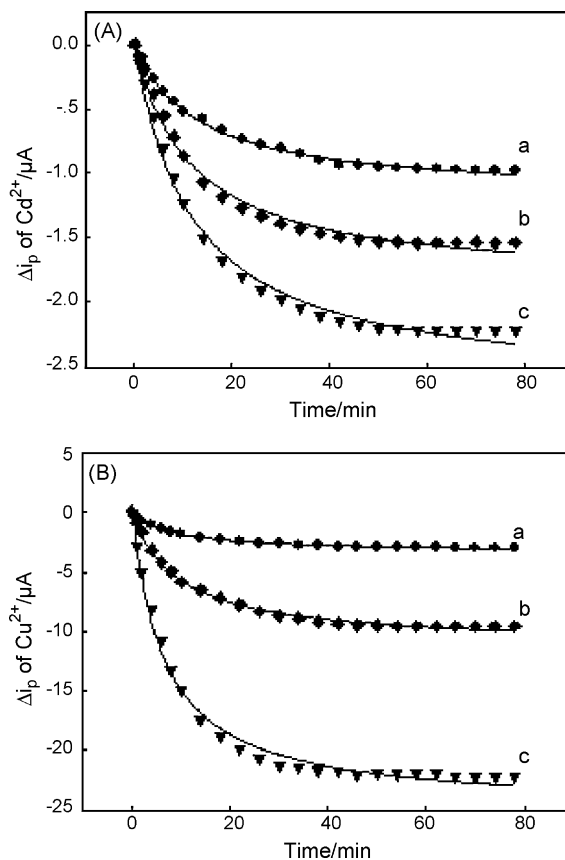


**Fig. 2.** (A) The  $\Delta i_p$  response with time for the binding process of cadmium to *P. aeruginosa* at different initial cadmium concentrations: (a) 10  $\mu\text{M}$ ; (b) 20  $\mu\text{M}$ ; (c) 40  $\mu\text{M}$ . (B) The  $\Delta i_p$  response with time for the absorption process of copper to *P. aeruginosa* at different initial copper concentrations: (a) 10  $\mu\text{M}$ ; (b) 20  $\mu\text{M}$ ; (c) 40  $\mu\text{M}$ .

### 3.5. The synchronous detection of cadmium and copper on the MES-modified electrode during the adsorption process

Inject *P. aeruginosa* solution (the final concentration is still 50  $\text{mg l}^{-1}$ ) into the electrochemical cell containing the detecting ions  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$ . In the same experiment, the initial concentrations of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  are the same. Fig. 3(A) and (B) respectively displays the  $\Delta i_p$  response with time during the binding process of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  onto *P. aeruginosa* at the initial concentrations of 10, 20 and 40  $\mu\text{M}$  from top to bottom.

Compared to the curves in Fig. 2, the ones in Fig. 3 display the same trend. The adsorption processes of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  onto *P. aeruginosa* act simultaneously, it is seen to have no obvious dif-



**Fig. 3.** (A) and (B) respectively shows the peak current with time response for the binding process of cadmium and copper to *P. aeruginosa* at different initial and cadmium copper concentrations: (a) 10  $\mu\text{M}$ ; (b) 20  $\mu\text{M}$ ; (c) 40  $\mu\text{M}$ .

ferentiation in time. However, there are some differences in the maximum of  $\Delta i_p$  and other factors in the two conditions.

### 3.6. Estimation of biosorption kinetics parameters

Taking  $k'_2$  and  $\Delta i_{p,\text{max}}$  as estimation parameters, the  $\Delta i_p$  in Figs. 2 and 3 is fitted by using the non-linear fitting program embedded in Sigmaplot Scientific Software Version 10.0. By fitting the experimentally obtained values to the electrochemical response model in Eq. (7), the kinetic parameters are obtained and listed in Tables 2–5, respectively. The correlation coefficients  $R^2$  in the four tables are all close to 1, which indicate that the metal ions in the condition of singleness and concomitance adsorbed onto *P. aeruginosa* can be described well by the pseudo-second-order kinetics

**Table 2**  
Kinetic parameters and regression coefficients ( $R^2$ ) for the biosorption of cadmium onto *P. aeruginosa* at various initial cadmium concentrations ( $C_0$ ) obtained by fitting the experimental values in Fig. 2(A) to Eq. (7) ( $\kappa = 0.01987 \mu\text{mol mg}^{-1} \mu\text{A}^{-1}$ ).

$C_0$ ( $\mu\text{M}$ )	$k'_2$ ( $\mu\text{A}^{-1} \text{min}^{-1}$ )	$-\Delta i_{p,\text{max}}$ ( $\mu\text{A}$ )	$k_2$ ( $\text{mg } \mu\text{mol}^{-1} \text{min}^{-1}$ )	$q_e$ ( $\mu\text{mol mg}^{-1}$ )	$R^2$
10	0.0928	0.903	0.5475	0.1137	0.9945
20	0.0488	1.653	0.2879	0.2553	0.9970
40	0.0447	2.199	0.2637	0.3230	0.9975

**Table 3**  
Kinetic parameters and regression coefficients ( $R^2$ ) for the biosorption of copper onto *P. aeruginosa* at various initial copper concentrations ( $C_0$ ) obtained by fitting the experimental values in Fig. 2(B) to Eq. (7) ( $\kappa = 0.01987 \mu\text{mol m}^{-1} \mu\text{A}^{-1}$ ).

$C_0$ ( $\mu\text{M}$ )	$k'_2$ ( $\mu\text{A}^{-1} \text{min}^{-1}$ )	$-\Delta i_{p,\text{max}}$ ( $\mu\text{A}$ )	$k_2$ ( $\text{mg } \mu\text{mol}^{-1} \text{min}^{-1}$ )	$q_e$ ( $\mu\text{mol mg}^{-1}$ )	$R^2$
10	0.0153	5.101	0.7700	0.1024	0.9974
20	0.00716	14.937	0.3603	0.2712	0.9960
40	0.00451	30.334	0.2270	0.5328	0.9937

**Table 4**

Kinetic parameters and regression coefficients ( $R^2$ ) for the biosorption of cadmium onto *P. aeruginosa* at various initial cadmium concentrations ( $C_0$ ) obtained by fitting the experimental values in Fig. 3(B) to Eq. (7) ( $\kappa = 0.01987 \mu\text{mol m}^{-1} \mu\text{A}^{-1}$ ).

$C_0$ ( $\mu\text{M}$ )	$k_2$ ( $\mu\text{A}^{-1} \text{min}^{-1}$ )	$-\Delta i_{p,\text{max}}$ ( $\mu\text{A}$ )	$k_2$ ( $\text{mg } \mu\text{mol}^{-1} \text{min}^{-1}$ )	$q_e$ ( $\mu\text{mol mg}^{-1}$ )	$R^2$
10	0.0569	1.173	0.3357	0.1522	0.9972
20	0.0468	1.852	0.2761	0.2822	0.9902
40	0.032	2.668	0.1888	0.3788	0.9927

**Table 5**

Kinetic parameters and regression coefficients ( $R^2$ ) for the biosorption of copper onto *P. aeruginosa* at various initial copper concentrations ( $C_0$ ) obtained by fitting the experimental values in Fig. 3(B) to Eq. (7) ( $\kappa = 0.01987 \mu\text{mol m}^{-1} \mu\text{A}^{-1}$ ).

$C_0$ ( $\mu\text{M}$ )	$k_2$ ( $\mu\text{A}^{-1} \text{min}^{-1}$ )	$-\Delta i_{p,\text{max}}$ ( $\mu\text{A}$ )	$k_2$ ( $\text{mg } \mu\text{mol}^{-1} \text{min}^{-1}$ )	$q_e$ ( $\mu\text{mol mg}^{-1}$ )	$R^2$
10	0.0351	3.366	1.7665	0.0773	0.9987
20	0.00933	11.171	0.4696	0.2073	0.9960
40	0.0062	24.917	0.3120	0.4406	0.9927

model. From the tables, it is also seen that the amount of metal ions adsorbed on to *P. aeruginosa* at equilibrium ( $q_e$ ) increases with the increasing initial metal ions concentrations.

Comparing Fig. 2(A) with Fig. 3(A) and Fig. 2(B) with Fig. 3(B), the results show that there are some differences in the value of  $q_e$  and other kinetics parameters. It is considered that there are some possible mutual influences when  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  as the detected metal ions are adsorbed synchronously by *P. aeruginosa*. In the concomitant condition of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$ , the value of  $\Delta i_{p,\text{max}}$  of  $\text{Cd}^{2+}$  is higher than that of unaccompanied with  $\text{Cu}^{2+}$ , and the corresponding  $q_e$  is also greater. As opposed to  $\text{Cd}^{2+}$ , the  $\Delta i_{p,\text{max}}$  and  $q_e$  of  $\text{Cu}^{2+}$  are lower in the concomitant condition. All mentioned above, due to the mutual influences between the two ions, the sorption of  $\text{Cd}^{2+}$  on *P. aeruginosa* is enhanced in the present of  $\text{Cu}^{2+}$ , which that of  $\text{Cu}^{2+}$  is weakened in the present of  $\text{Cd}^{2+}$ . The mutual influences here are competitive and restraining relationship. Table 6 shows the changing percentage of  $q_e$  of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  in the concomitant condition vs. the unaccompanied term.

3.7. The characteristics adsorption isotherms for  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  onto *P. aeruginosa*

It is significant for studying the biosorption mechanism and designing biologic reaction to analyze the characteristics of adsorption isotherms. In this work, the adsorption characteristics of the cadmium and copper onto *P. aeruginosa* are described by the Langmuir [23] and the Freundlich [24] adsorption isothermal models, which can indicate the quantitative relation between  $q_e$  and  $C_e$  expressed respectively in Eqs. (8) and (9):

$$q_e = \frac{q_{\text{max}} C_e}{K_d + C_e} \tag{8}$$

$$q_e = K_f C_e^{1/n} \tag{9}$$

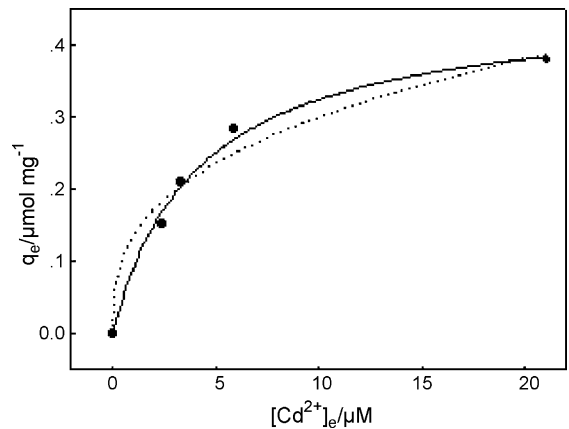
where  $q_{\text{max}}$  ( $\mu\text{mol mg}^{-1}$ ) is the maximum adsorption capacity and  $K_d$  ( $\mu\text{M}$ ) is the dissociation constant depending to the stability of metal–biosorbent complexes,  $n$  is the Freundlich constant with no dimension, and  $K_f$  ( $1 \text{ mg}^{-1}$ ) is a constant related to the adsorption capacity.

Fig. 4 shows the adsorption isotherms of  $\text{Cd}^{2+}$  onto *P. aeruginosa* in the solution with both  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  as the detected ions.

**Table 6**

The changing percentage of  $q_e$  in the solution containing the two cations compared to in the solution with either.

$C_0$ ( $\mu\text{M}$ )	$\Delta q_e$ (%) ( $\text{Cd}^{2+}$ )	$\Delta q_e$ (%) ( $\text{Cu}^{2+}$ )
10	+33.84%	–24.52%
20	+10.55%	–23.58%
40	+17.28%	–17.30%



**Fig. 4.** Isotherms of cadmium in the competitive absorption process onto *P. aeruginosa*: (a) simulation with Langmuir isotherm model, (b) simulation with Freundlich isotherm model.

It is noticed that the values of  $q_e$  increase with the increasing  $C_e$  values. Similarly, the adsorption isotherms in other conditions also can be obtained and fitted by the two models. And the corresponding parameters and correlation coefficients are listed in Table 7, respectively.

From Table 7, it is determined that the two theoretic models can well depict the adsorption isotherms for  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  under all conditions in this work. And the competitive and restraining relations are also revealed obviously.

3.8. Reuse of *P. aeruginosa*

The reusability of the biosorbent was also investigated. For this test, *P. aeruginosa* loaded with  $\text{Cd}^{2+}$  was treated with a 1 M  $\text{HNO}_3$  solution in order to desorb the  $\text{Cd}^{2+}$ . The biomass was separated by centrifugation, washed several times with deionized water and then reused for the  $\text{Cd}^{2+}$  adsorption. This process was repeated five

**Table 7**

Biosorption isotherm constants for the biosorption of cadmium and copper onto *P. aeruginosa* at 20 °C.

	Langmuir			Freundlich		
	$q_{\text{max}}$ ( $\mu\text{mol m}^{-1}$ )	$K_d$ ( $\mu\text{M}$ )	$R^2$	$K_f$ ( $1 \text{ mg}^{-1}$ )	$n$	$R^2$
<sup>a</sup> $\text{Cd}^{2+}$	0.4269	6.8134	0.9673	0.0928	2.4740	0.9481
<sup>a</sup> $\text{Cu}^{2+}$	0.8975	3.0762	0.9927	0.2078	2.4093	0.9673
<sup>b</sup> $\text{Cd}^{2+}$	0.4589	4.1420	0.9944	0.1352	2.8902	0.9741
<sup>b</sup> $\text{Cu}^{2+}$	0.7541	3.4131	0.9876	0.1792	1.9707	0.9655

<sup>a</sup> $\text{Cd}^{2+}$  is in the solution containing only  $\text{Cd}^{2+}$  detected. <sup>a</sup> $\text{Cu}^{2+}$  is in the solution containing only  $\text{Cu}^{2+}$  detected. <sup>b</sup> $\text{Cd}^{2+}$  and <sup>b</sup> $\text{Cu}^{2+}$  are in the competitive absorption system.

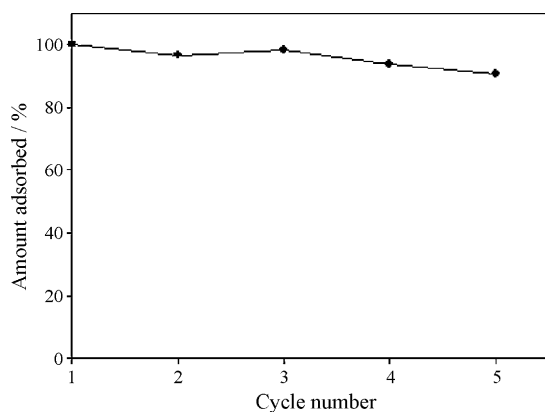


Fig. 5. Reuse of *P. aeruginosa* for sorption/desorption of  $\text{Cd}^{2+}$ . The amount of  $\text{Cd}^{2+}$  adsorbed at the first time was considered as 100%.

times and the result was shown in Fig. 5. As can be seen, this biosorbent exhibited excellent reusability. The absorption capacity had not decreased obviously after five adsorption/desorption cycles.

#### 4. Conclusion

In this work, a sensitive and effective electrode system was successfully developed for the simultaneous determination of  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  during the adsorption process onto *P. aeruginosa* by SWASV. The gold electrode was modified with a selectively porous MES monolayer, and the free metal ions were detected free from macromolecule contaminants. For the real-time detection without any pretreatment, the adsorption process was successfully monitored, the adsorption kinetic parameters were obtained by fitting with the pseudo-second-order kinetic model, and the adsorption characteristics in the conditions including separate existence and co-exist of the two metal ions were also studied. Furthermore, the Langmuir and the Freundlich adsorption isothermal models well described the adsorption processes in this work due to the high correlative coefficients. By comparing the amount of metal ion adsorbed at equilibrium ( $q_e$ ) and other kinetics parameters, a competitive and restraining relationship between  $\text{Cd}^{2+}$  and  $\text{Cu}^{2+}$  during the simultaneous adsorption process was revealed and discussed. The novel method used to study various metal ions adsorption system in the present work provided a new approach to simultaneous detection of trace metal ions in complex biosorption process.

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